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Keywords

sulfated zirconia, mesoporous, SBA-15, cellobiose, hydrolysis, biomass, Schuit Institute of Catalysis

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Keywords Sulfated zirconia · Mesoporous · SBA-15 · Cellobiose · Hydrolysis · Biomass

1 Introduction

So far, considerable effort has been dedicated for the economic production of ethanol as it is an excellent alternative transportation fuel and can be blended with gasoline [1, 2]. However, ethanol is currently produced from sugar cane and the starch portion of corn, competing with food production, thus raising ethical concerns [3]. It is also very important to develop technologies for the efficient utilization of cellulose, a major constituent of lignocellulosic agricultural residues, as one of the renewable sources of chemicals [4, 5]. Cellulose is a polymer of glucose monomers connected by β -1,4-glycosidic bonds. It can be hydrolyzed to glucose through enzymatic or acid hydrolysis [6, 7]. The advantage of the enzymatic route is the absence of the degradation products but the reactions proceed rather slowly and separation is cumbersome [8]. Mineral acids can depolymerize cellulose into individual glucose units, accompanied by degradation products such as furfural, hydroxymethylfurfural and tar-like products. These side products are toxic for the microorganisms used for further fermentation of the glucose product. Recovery of the mineral acids is another challenge and in any case mineral acids are not desired because of their corrosive nature [9]. In order to overcome these drawbacks, heterogeneous catalytic systems have been proposed [10–17]. The conversion of cellulose into glucose and the simultaneous hydrogenation of glucose into sugar alcohols, such as sorbitol and mannitol on Ru/C [11], polymer stabilized Ru nanoclusters [12], and Pt and Ru supported by HUSY and γ -Al₂O₃ [13] has been reported. In order to replace the mineral acids in the acid hydrolysis of cellulose, solid acid catalysts such as sulfonated activated carbon (AC-SO₃H) [14], sulfonic acid-mesoporous materials [15, 16], and Brønsted acidic zeolites [13, 14] were used. Higher glucose yields were reported for

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sulfate modified catalysts than for acidic zeolites. Besides in the hydrolysis of sucrose and starch, sulfonated mesoporous silicas showed higher activities than ion exchange resins and HZSM-5 catalysts [17]. In this sense, sulfated zirconia is expected to show high glucose yields, albeit a significant amount of by-products has been noted [14].

The textural properties of conventional sulfated zirconia are not beneficial with relatively low surface areas (100–120 m²/g). Much effort has been spent in order to prepare a high surface area sulfated zirconia. Mesoporous silicas have attracted wide-spread interest due to the high surface area (up to 1000 m²/g), large pore volume, and a hexagonal array of uniform pores. The silanol groups on the surface of these materials are neutral or slightly acidic. Combining these beneficial textural properties of ordered mesoporous silicas with the intrinsic acidity of sulfated zirconia by dispersing the latter in the former would greatly enhance the catalytic activity. SBA-*n* mesoporous materials [18, 19] have higher stability than other typical mesoporous silicas such as of the M41S family [20] due to their thicker walls, which should be beneficial when the aim is to introduce other components into the framework. The introduction of the zirconia precursor simultaneously with the silicon precursor in the preparation of SBA-15 was shown to be effective for a good distribution of zirconium within the silica framework [21].

In our previous work, we have found indications for strong Brønsted acidity of sulfate modified ZrO₂/SBA-15 by ¹H MAS NMR [22]. The origin of the strong surface acidity in sulfated zirconia has not been unequivocally resolved [23, 24]. Several postulates on the acidity, whether it is related to the sulfate group and various binding structures of this group to the zirconia surface, have been proposed [25–31]. Here, we investigated the surface acidity of a range of ZrO₂/SBA-15 composites by infrared spectroscopy of adsorbed carbon monoxide. In addition, temperature-programmed decomposition of adsorbed alkylamines was used to probe the density of surface acidic sites. It is known that alkyl ammonium ions form upon protonation of amines by Brønsted sites and decompose into the corresponding alkene and NH₃ in a narrow temperature range through a reaction similar to the Hoffman elimination [32]. The hydrolysis reactivity of a range of ZrO₂/SBA-15 composites was determined using cellobiose as a model substrate. Cellobiose is a dimer of glucose with β-1,4-glycosidic bonds, providing a useful model compound for the hydrolysis of cellulose.

2 Experimental

2.1 Synthesis of Materials

SBA-15 silica materials were prepared by a well-established procedure [18, 19]. Siliceous SBA-15 was prepared

by adding 9 ml of tetraethyl orthosilicate (TEOS) to 150 ml of 1.5 M HCl solution containing 4 g of Pluronic-123 (Aldrich). The mixture was stirred for 24 h at 40 °C and allowed to further react at 100 °C overnight in Teflon bottles. Subsequently, the solid material was obtained by filtration, dried at room temperature overnight and calcined at 500 °C in an air flow for 5 h. Zirconium was introduced in the synthesis solution simultaneously with TEOS in the form of zirconiumoxychloride (ZrOCl₂·8H₂O, 99.9%, Strem Chemicals). Appropriate amounts of the zirconium precursor were added to obtain final products with 5–25:100 ZrO₂:SiO₂ ratios. The materials are denoted as Zr(*x*)SBA-15 with *x* being the ZrO₂ M amounts per 100 mol SiO₂. Sulfated catalysts were prepared by sulfation in a 0.25 M H₂SO₄ solution for 15 min followed by drying overnight at 80 °C. The sulfated catalysts were activated at 350 °C for 3 h in static oven to remove the physisorbed sulfur species. Al-SBA-15 was prepared by prehydrolysing 0.25 g aluminum iso-propoxide (Acros Organics, 98%) in 10 ml of HCl solution. This solution was then added to the synthesis gel of SBA-15 to obtain Al-SBA-15. The Si/Al ratio is 34 in the final catalyst with a surface area of 903 m²/g. Conventional sulfated zirconia was prepared by calcination of the sulfated zirconium hydroxide provided by MEL Chemicals (XZO 1249/01) at 500 °C for 5 h.

2.2 Characterization

Elemental analyses were carried out by ICP-OES (Spectro Ciros CCD ICP optical emission spectrometer with axial plasma viewing). To extract the metals, the catalysts were dissolved in a 1.5 ml solution of HF/HNO₃/H₂O (1:1:1) acid mixture.

TEM images were taken on a FEI T20 electron microscope operating at 200 kV. The specimens were dispersed in ethanol and placed on holey copper grids.

The surface areas were measured using nitrogen adsorption isotherms at –196 °C on a Micromeritics ASAP 2000 gas sorption and porosimetry system. The samples were prepared for measurement by degassing at 150 °C for 24 h. Surface areas were calculated by the BET (Brunauer-Emmett-Teller) method and the pore volumes were determined by using the BJH (Barrett-Joyner-Halenda) method by using the adsorption cumulative volume of pores between 1.7 and 100 nm.

FT-IR spectra of the samples were recorded in the range of 4000–400 cm⁻¹ by a Bruker IFS 113v instrument. The spectra were acquired at a 2 cm⁻¹ resolution and averaged over 20 scans. The samples were prepared as thin self-supporting wafers of 5–10 mg/cm² and placed inside a controlled environment infrared transmission cell, capable of heating and cooling, gas dosing and evacuation. Prior to CO adsorption, the catalyst wafer was heated to 450 °C at a

rate of 10 °C/min in an oxygen atmosphere. Subsequently, the cell was out-gassed at the final temperature until the residual pressure was below 5×10^{-5} mbar. The sample was then cooled to -190 °C. CO was introduced into the cell via a sample loop (0.4 μmol per dose) connected to a Valco six-port valve.

Temperature programmed decomposition (TPD) of *i*-propylamine (IPAm) was performed in a packed-bed quartz reactor. The effluent gases were analyzed by a Balzers quadrupole mass spectrometer. 100 mg of catalyst was heated at a rate of 5 °C/min to 450 °C in a He flow of 100 ml/min. The sample was then cooled to 100 °C and exposed to excess gaseous IPAm (99.5%, Aldrich) for 10 min. Physisorbed IPAm was removed at 100 °C by purging in 100 ml/min He for 24 h. TPD of IPAm was carried out by heating the sample to 550 °C at a rate of 5 °C/min in 200 ml/min He. The formation of propene ($m/e = 41$) and ammonia ($m/e = 17$), i.e. the decomposition products of IPAm, as well as the amount of desorbed IPAm ($m/e = 44$, 41, and 17) were followed and compared to well-calibrated standards. The TPD curves were carefully deconvoluted and the peak areas were used to determine the relative contributions.

2.3 Catalytic Activity

Cellobiose hydrolysis was carried out in a lab-scale batch reactor (Autoclave Engineers, 100 ml). Typically, the reactor was charged with a 50 ml solution of 0.5 wt% cellobiose in water to which a predetermined amount of catalyst (0.1 wt% compared to solvent) was added. Kinetic experiments were performed at 160 °C under a nitrogen pressure of 20 bar. Nitrogen overpressure was employed to ensure that the reaction medium (water) remained as liquid

during the reaction. The start of the reaction was taken as the moment when the reactor contents reached the desired reaction temperature. Although the reactors were heated as fast as possible, heating took about 10 min, during which period some reaction already took place. When the loss of cellobiose was traced during heating, it was found that the loss was not more than 10% for each catalytic system under study amounting significantly lower than the initial rates. Samples were withdrawn every 30 min for 1.5 h. Analysis was performed offline using a Waters HPLC system equipped with a H^+ -column (Polymer Lab.) and RI detector. The column temperature was kept constant at 60 °C. The mobile phase was 10 mM sulfuric acid solution which was fed at a flow rate of 0.6 ml/min. The glucose and the cellobiose concentrations were determined from calibration curves prepared by using external standards.

The sulfur elution of the catalysts were determined at the reaction conditions as well. In a typical test, 10 mg catalyst was added to 5 ml of water for 0–60 min at 160 °C. The catalyst was recovered by centrifugal separation under vacuum and the elemental analysis was performed by using a Perkin-Elmer Series II 2400 CHNS analyzer.

3 Results and Discussion

3.1 Physicochemical Properties

The intended compositions, Zr and S contents determined from the elemental analysis, SO_4/Zr ratio and BET surface areas of the catalysts are collected in Table 1. Pure SBA-15 has a surface area of nearly 800 m^2/g , which is consistent

Table 1 Zirconia and sulfur contents of the catalysts determined by elemental analysis and the BET surface area of the non-sulfated and sulfated Zr-SBA-15

Catal	Si/Zr		Zr (wt%)	S (wt%)	SO_4/Zr molar ratio	BET surface area (m^2/g)	Pore volume (cc/g)
	Gel	Product					
SBA-15	na ^a	na	na	na	na	773	1.18
Zr(15)SBA-15	7	26	5.3	na	na	586	1.46
Zr(25)SBA-15	4	11	10.9	na	na	506	1.15
SZr(5)SBA-15	20	33	4.3	3.5	2.3	313	0.43
SZr(10)SBA-15	10	39	3.7	3.4	2.6	311	0.43
SZr(15)SBA-15	7	27	5.2	3.4	1.9	284	0.40
SZr(20)SBA-15	5	15	8.9	3.2	1.1	261	0.39
SZr(25)SBA-15	4	12	10.8	3.3	0.9	246	0.34
SZr(30)SBA-15	3	13	13.4	3.1	0.7	203	0.24
SZ-Commercial	na	na	na	7.0 ^b	0.22	123	0.10
Al-SBA-15	na	na	na	na	na	903	1.11

^a Not applicable

^b Before calcination

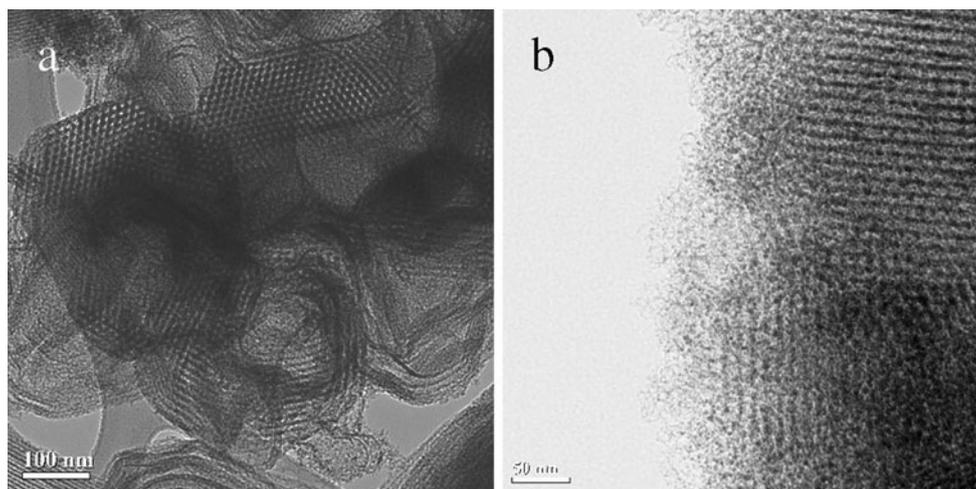


Fig. 1 Electron micrographs of **a** SBA-15 and **b** SZr(15)SBA-15

with the highly ordered mesostructure seen from TEM image (Fig. 1). Upon introduction of zirconia, the BET surface areas decreased to values between 500 and 600 m²/g, indicating that the introduction of zirconia in SBA-15 has resulted in a less ordered structure than siliceous SBA-15. The zirconium contents in the calcined materials were lower than the amounts in the synthesis gel, implying that not all Zr was built into SBA-15 and remained dissolved in the synthesis solution. Initially, we used 1 M H₂SO₄ to sulfate the Zr(x)SBA-15 materials, but this had a strong adverse effect on the textural properties (surface areas below 100 m²/g). A sulfuric acid concentration of 0.25 M was sufficient to provide good sulfation without causing too much loss of surface area. The surface area of the sulfated Zr(x)SBA-15 materials was above 200 m²/g and still higher than that of conventional sulfated zirconia. The sulfur content of the calcined sulfated samples was about 3.3 wt% and did not change much with the Zr content. The SO₄/Zr ratio decreases with Zr content. While this ratio is in excess of 2 at low Zr content, it decreases strongly above a Zr content of 5 wt%. This may point to the gradual agglomeration of Zr ions into larger domains, of which only the outer surface can be sulfated. The XRD patterns did not show clear reflections in the low angle region for the zirconium-containing samples, indicating that the long range order of mesopores was absent. No reflections were observed in the high-angle region, implying that either the zirconium atoms were well dispersed or that the zirconia domains remain very small. Elemental analysis of the catalysts at various time under hydrothermal conditions at 160 °C (Table 2) indicated that a substantial part of the sulfur species are eluted under reaction conditions in the commercial sulfated zirconia catalyst as well as the SZr(x)SBA-15 catalysts.

Table 2 Sulfur contents of the catalysts after hydrothermal treatment at 160 °C determined by elemental analysis

Catalyst	S (wt%)			
	0 (min)	10 (min)	30 (min)	60 (min)
SZr(15)SBA-15	3.40	0.30	0.20	0.20
SZr(25)SBA-15	3.30	0.30	0.21	0.20

3.2 Infrared Spectroscopy of Adsorbed Carbon Monoxide

A FT-IR spectrum in the CO stretching region of SBA-15 after carbon monoxide adsorption at liquid nitrogen temperature is shown in Fig. 2a. The spectra exhibit two distinct bands at 2138 and 2158 cm⁻¹. The latter is attributed to CO adsorbed on weakly acidic silanol groups. The band at 2138 cm⁻¹ is due to a weakly perturbed condensed carbon monoxide phase on the surface of SBA-15 [33, 34]. The weak feature at 2110 cm⁻¹ derives from carbon monoxide coordinating with its oxygen atom to the silanol group. The FT-IR spectra in the CO stretching region of Zr(15)SBA-15 catalyst are given in Fig. 2b. In the presence of zirconia, an additional band at 2185 cm⁻¹ was also observed. This band was assigned to Lewis acid sites formed by coordinatively unsaturated Zr⁴⁺ sites [32]. Increasing CO coverage saturated these sites earlier than the silanol groups, implying that the former sites bind CO stronger than the latter in accordance with the larger shift of the carbon monoxide stretching frequency.

Infrared spectra of CO adsorption on SZr(15)SBA-15 are shown in Fig. 2c. Similar to the non-sulfated catalyst, a band at 2138 cm⁻¹ was observed due to the weakly physisorbed CO. The band around 2160 cm⁻¹ was

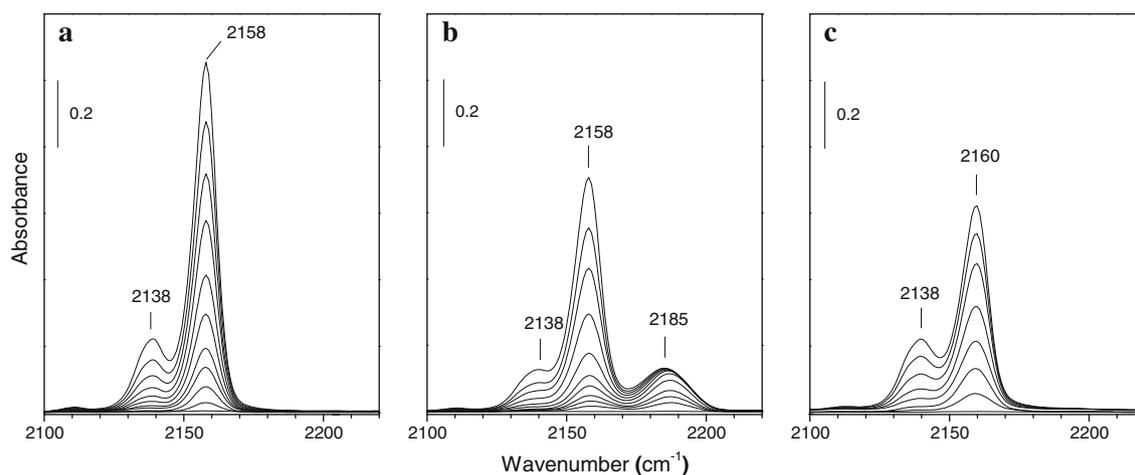
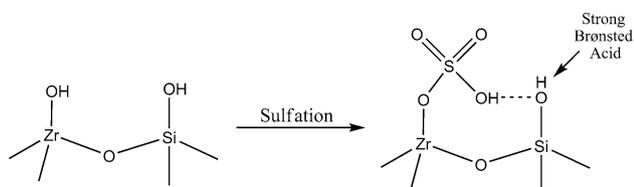


Fig. 2 FT-IR spectra of adsorbed carbon monoxide at liquid nitrogen temperature for **a** SBA-15, **b** Zr(15)SBA-15 and **c** SZr(15)SBA-15 upon increasing CO coverage (doses of 0.4 μmol CO)



Scheme 1

attributed to CO adsorbed on silanol groups. It was located at a slightly higher wavenumber than that in SBA-15 and Zr(15)SBA-15 ($\nu_{\text{CO}} = 2158 \text{ cm}^{-1}$). The band at 2186 cm^{-1} due to CO coordinating to low coordinated Zr^{4+} sites disappeared on sulfated samples. This was attributed to complete coverage of the Lewis acid sites by sulfate groups. Scheme 1 gives a schematic representation of the low coordinated Zr^{4+} sites and silanol groups on the surface of the Zr-SBA-15 catalysts and the suggested formation of strong acid groups in the presence of sulfate groups for SZr-SBA-15 catalysts.

The infrared spectra of CO adsorption on conventional sulfated zirconia are shown in Fig. 3. The band at 2170 cm^{-1} was attributed to the CO adsorbed on terminal hydroxyl groups on the zirconia surface. The high frequency band was red-shifting with increasing CO coverage in the region between 2192 and 2205 cm^{-1} . This band was assigned to the C–O stretching mode of carbon monoxide interacting with Lewis acid sites, i.e. the Zr^{4+} sites, of varying acidity.

The infrared spectra in the silanol stretching region of SBA-15, Zr(15)SBA-15 and SZr(15)SBA-15 catalysts are shown in Fig. 4a–c, respectively. The spectrum of SBA-15 (Fig. 4a) exhibits a sharp feature at 3747 cm^{-1} which is ascribed to the isolated, non-hydrogen bonded silanol groups on the surface. The broad tail extending towards 3400 cm^{-1} is due to the hydrogen bonded silanol groups.

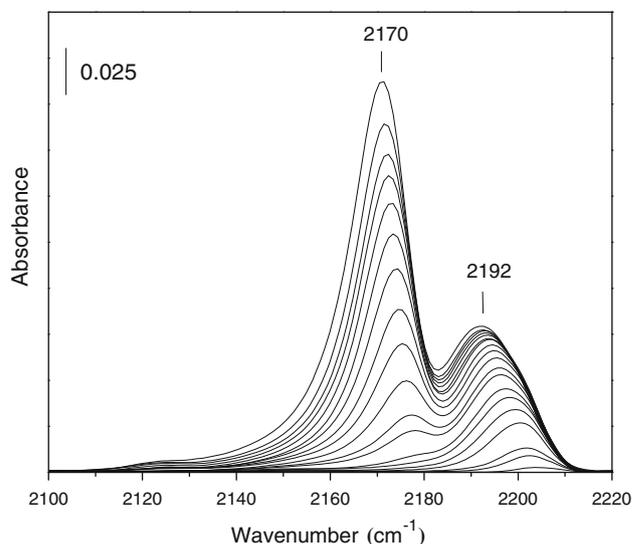
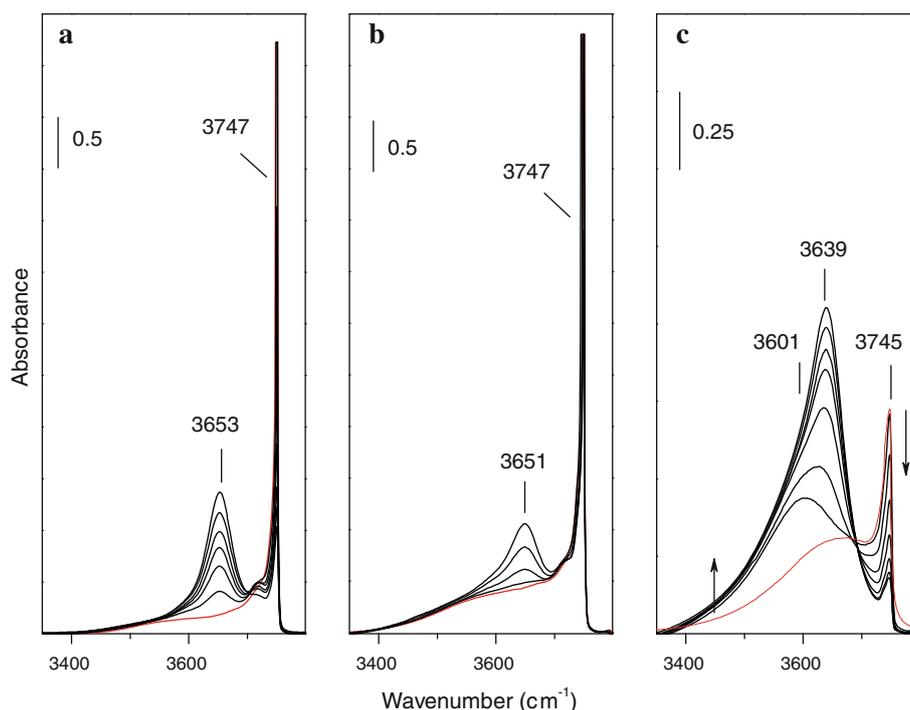


Fig. 3 FT-IR spectra of adsorbed carbon monoxide at liquid nitrogen temperature for commercial sulfated zirconia upon increasing CO coverage (doses of 0.4 μmol CO)

CO adsorption on isolated silanol groups weakens the hydroxyl bond and leads to a perturbed band around 3653 cm^{-1} with a frequency shift of 94 cm^{-1} . The silanol stretching region of the Zr(15)SBA-15 catalyst (Fig. 4b) is similar to pure SBA-15 with the exception of a very weak feature around 3794 cm^{-1} attributed to isolated terminal hydroxyl groups bonded to Zr. The shift of the hydroxyl groups upon CO adsorption is very similar to SBA-15. This indicates the silanol groups are still only weakly acidic in the zirconia-substituted SBA-15.

The corresponding hydroxyl region for SZr(15)SBA-15 is shown in Fig. 4c. The intensity of the band at 3747 cm^{-1} is less pronounced than the intensity of the corresponding bands on SBA-15 or Zr/SBA-15 samples. The IR spectra as

Fig. 4 FT-IR spectra of adsorbed carbon monoxide at liquid nitrogen temperature in the hydroxyl stretching region for **a** SBA-15, **b** Zr(15)SBA-15 and **c** SZr(15)SBA-15 upon increasing CO coverage (doses of 0.4 $\mu\text{mol CO}$). The *red line* represents the spectra before the addition of CO. The *arrow* indicates the increasing CO coverage



a function of CO coverage clearly evidence the presence of two types of silanol groups. At low CO coverage, part of the hydroxyl band at 3745 cm^{-1} is shifted to 3601 cm^{-1} , corresponding to a shift of 144 cm^{-1} . With increasing CO coverage, the band of perturbed OH broadens and $\Delta\nu_{\text{OH}}$ at high CO coverage is 106 cm^{-1} . The evolution of the spectra evidence the presence of stronger acidic sites giving rise to $\Delta\nu_{\text{OH}} = 144 \text{ cm}^{-1}$ next to weakly acidic sites ($\Delta\nu_{\text{OH}} = 94 \text{ cm}^{-1}$). An IR frequency shift of 144 cm^{-1} upon CO adsorption on SZr(15)SBA-15 is very close to the 139 cm^{-1} shift reported earlier for a conventional sulfated zirconia catalyst [35].

Previous FT-IR investigations provide evidence that sulfation of zirconia enhances the strength of the bridging zirconia hydroxyl groups, that is Zr-(OH)-Zr, and eliminates the terminal ones (i.e., ZrOH) [27]. In addition, it creates a new type of Brønsted acid site, presumably protons forming multicentered or single bonds with sulfate ions. These protons are hydrogen bonded to the surface [28]. Similarly, when zirconia included SBA-15 was modified by sulfation, the Lewis acid sites were covered by sulfate groups and the terminal hydroxyls of zirconia were eliminated (Fig. 5). As a result of the interaction of these sulfate ions with the silanol groups, strong Brønsted acidity is developed.

The presence of strong Brønsted acidity was indicated by the sulfate and the silanol stretching regions. The red shift ($\Delta\nu_{\text{OH}} = 144 \text{ cm}^{-1}$) observed in the silanol stretching region for SZr-SBA-15 catalysts upon CO adsorption is similar to that for conventional sulfated zirconia reported in literature ($\Delta\nu_{\text{OH}} = 139 \text{ cm}^{-1}$) [35]. This suggests that our

catalysts have similar acidity as conventional sulfated zirconia. The $\Delta\nu_{\text{OH}}$ of 144 cm^{-1} is higher than the shift for weakly acidic silanol, yet lower than that of strongly acidic zeolites (stabilized faujasite zeolite, $\Delta\nu_{\text{OH}} \approx 300 \text{ cm}^{-1}$) [36, 37]. The IR spectra of the S=O stretching region for SZr(15)SBA-15 are presented in Fig. 6. CO adsorption brings about a positive frequency shift of about 26 cm^{-1} . This shift indicates an increase of the S=O bond strength and is attributed to the interaction of CO with the strongly acidic proton, as weakening of the SO-H bond upon interaction of the proton with CO causes an increase of the S=O bond strength. This observation provides an indirect indication for the presence of protonic sites connected to the sulfate groups. Indeed, direct observation of the strong Brønsted acid protons in sulfated zirconia catalysts is not straightforward, likely because of the strong hydrogen bonding to adjacent surface groups [22].

3.3 Temperature-Programmed Decomposition of IPAm

The evolution of propene during temperature programmed IPAm decomposition for the various catalysts is shown in Fig. 7. No IPAm decomposition is observed for siliceous SBA-15. For the zirconia-containing catalysts, decomposition of adsorbed IPAm takes place between 310 and 360 $^{\circ}\text{C}$ with a maximum around 340 $^{\circ}\text{C}$. In contrast, the decomposition in the sulfated catalysts occurred in the interval 290–340 $^{\circ}\text{C}$ with a maximum around 312 $^{\circ}\text{C}$. In Table 3, the amounts of decomposed IPAm as well as the

Fig. 5 FT-IR spectra of adsorbed carbon monoxide at liquid nitrogen temperature in ZrOH stretching region for **a** non sulfated Zr(25)SBA-15 and **b** sulfated Zr(25)SBA-15 upon increasing CO coverage (doses of 0.4 $\mu\text{mol CO}$)

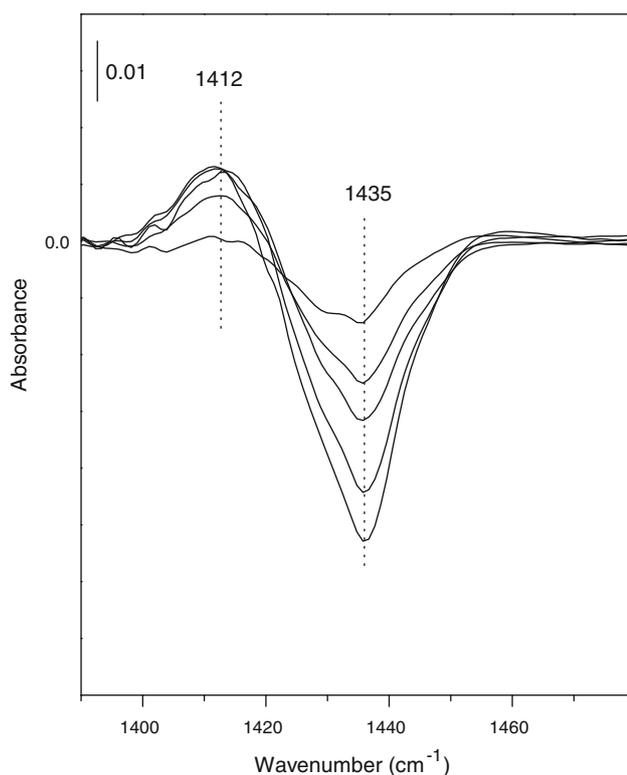
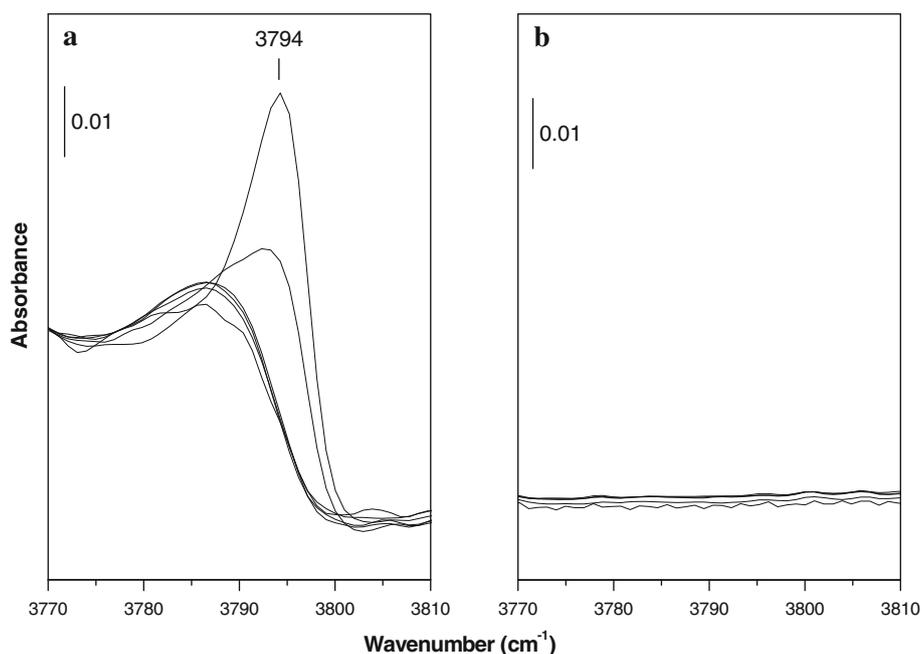


Fig. 6 FT-IR spectra of adsorbed carbon monoxide at liquid nitrogen temperature in the region of S=O stretch for SZr(15)SBA-15 upon increasing CO coverage (doses of 0.4 $\mu\text{mol CO}$)

decomposition temperature are given for these catalysts. Introduction of zirconia in the silica results in the creation of sites capable of chemisorbing and decomposing IPAm.

Upon sulfation, the decomposition temperature for Zr(15)SBA-15 decreases considerably. The difference is due to the increased acidity of the catalysts. This leads to activation of the chemisorbed IPAm complex at lower temperature. Table 3 also gives the results for two reference samples HZSM-5 and Al-SBA-15. The former contains exclusively aluminum in the zeolite framework and the amount of IPAm decomposed corresponds to the aluminum density. The latter contains mainly Lewis acidic Al sites on the surface of SBA-15. IPAm chemisorbed to these Lewis acidic sites decomposes at a higher temperature and the result is very similar to that of the non-sulfated Zr(x)/SBA-15 samples. It is then straightforward to conclude that IPAm in the non-sulfated catalyst adsorbs to Lewis acid Zr^{4+} sites, whereas this adsorption state should be absent after sulfation. Instead, the Brønsted acidic sites adsorb IPAm more strongly through protonation of the alkylamine, which results in a lower decomposition temperature. For the series of sulfated Zr(x)/SBA-15, the amount of decomposed IPAm first increases up to a value of 0.5 mmol/g for SZr(15)SBA-15 and then decreases with increasing Zr content. The increase of the acidity at lower Zr content indicates the increase of the number of Zr ions in or at the SBA-15 surface and points to their dispersed nature. At higher Zr content, zirconia domains are formed, which have a lower number of Zr ions at their surface. This is in line with the lower SO_4/Zr ratios. In principle, the decrease of the acidity with increasing Zr content may thus be due to the formation of segregated domains of zirconia. An additional reason may lie in the importance of the interaction of sulfate groups attached to Zr ions with silanol groups in acidity generation as indicated by the IR results.

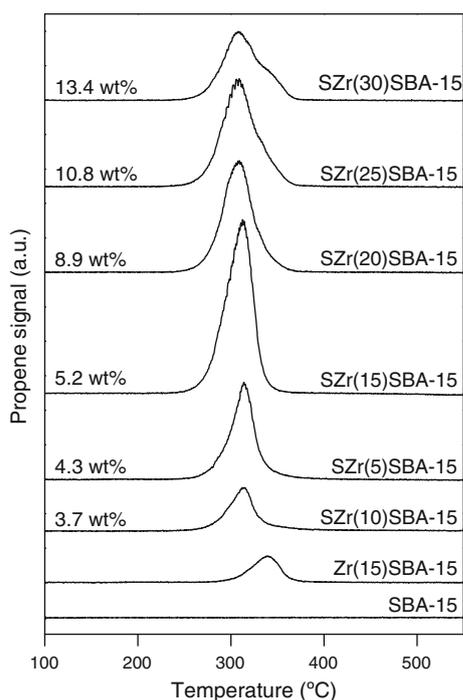


Fig. 7 Production of propene from *i*-propylamine decomposition during TPD for the various catalysts. Actual Zr loadings determined by elemental analysis for zirconium-containing silicas are indicated left

Obviously, agglomeration of Zr at the surface of SBA-15 results in a decrease of the interaction of the grafted sulfate with the silanol groups and may thus decrease overall acidity. For SZr(20)SBA-15 and the samples with higher Zr loading, we find that there are two peaks in propene production, one main peak around 310 °C and the other smaller contribution around 340 °C. The contribution of the latter peak increases somewhat with the zirconium loading. As its location is similar to the peak observed for the non-sulfated sample, we infer that these samples contain a small amount of Lewis acidic Zr^{4+} sites.

3.4 Catalytic Activity

The conversion of cellobiose and the yield to glucose at a reaction temperature at 160 °C are given in Fig. 8. Comparing the SBA-15 based catalysts; the sulfated catalysts are more active in cellobiose conversion. The cellobiose conversion is about 80% after 90 min for SZr(15)SBA-15 and SZr(25)SBA-15. In comparison, Zr(15)SBA-15 displays a much lower activity. The activity of an Al-SBA-15 reference catalyst is also very low. The lower activities of Zr(15)SBA-15 imply that the hydrolysis of cellobiose is more favorable on Brønsted acid sites than on Lewis acid sites. The activity of the conventional sulfated zirconia material is very close to the sulfated Zr(*x*)SBA-15 materials. On the other hand, the glucose yields of the sulfated Zr(*x*)SBA-15 are much higher than conventional sulfated zirconia. Catalysts with Brønsted acid sites showed high selectivity for glucose in previous studies [16, 38]. Hence, the higher yields of glucose on sulfated Zr(*x*)SBA-15 in comparison to conventional sulfated zirconia is most likely due to the small amount of Lewis acid sites, known to catalyze the dehydration of glucose. The hydrolysis reactions are generally followed by glucose degradation reactions, including condensation, fragmentation and resinification reactions producing polyacids, sugar derivatives and polymeric residues [14]. Therefore, we limit ourselves here to follow cellobiose conversion and glucose yield.

The sulfur content of all the catalysts decreased under reaction conditions. A comparison of the two composite catalysts SZr(15)SBA-15 and SZr(25)SBA-15 shows that the sulfur contents during catalytic operation are very similar (Table 2). The SZr(15)SBA-15 catalyst is more active and this is undoubtedly related to the higher amount of Brønsted acid sites. Our IPAm decomposition results show that the SZr(15)SBA-15 catalyst has the highest Brønsted acidity content. The incorporation of sulfated zirconia into SBA-15 structure does not substantially improve hydrothermal stability as sulfur species leach during reaction.

Table 3 IPAm decomposition temperatures and amounts for different catalysts

Catalyst	Zr loading (wt%)	$N_{IPAm, total}$ (mmol/g cat.)	$T_{max,1}$ (°C)	$N_{IPAm,1}$ (mmol/g cat.)	$T_{max,2}$ (°C)	$N_{IPAm,2}$ (mmol/g cat.)
SBA-15	–	0.0	–	–	–	–
Zr(15)SBA-15	5.3	0.09	–	–	340	0.09
SZr(5)SBA-15	4.3	0.26	314	0.26	–	–
SZr(10)SBA-15	3.7	0.14	313	0.14	–	–
SZr(15)SBA-15	5.2	0.50	313	0.50	–	–
SZr(20)SBA-15	8.9	0.37	307	0.36	342	0.01
SZr(25)SBA-15	10.8	0.39	308	0.36	341	0.03
SZr(30)SBA-15	13.4	0.27	308	0.23	342	0.04
HZSM-5 ^a	–	0.82	310	0.82	–	–
Al-SBA-15 ^b	–	0.09	345	0.09	–	–

^a Si/Al = 20

^b Si/Al = 34

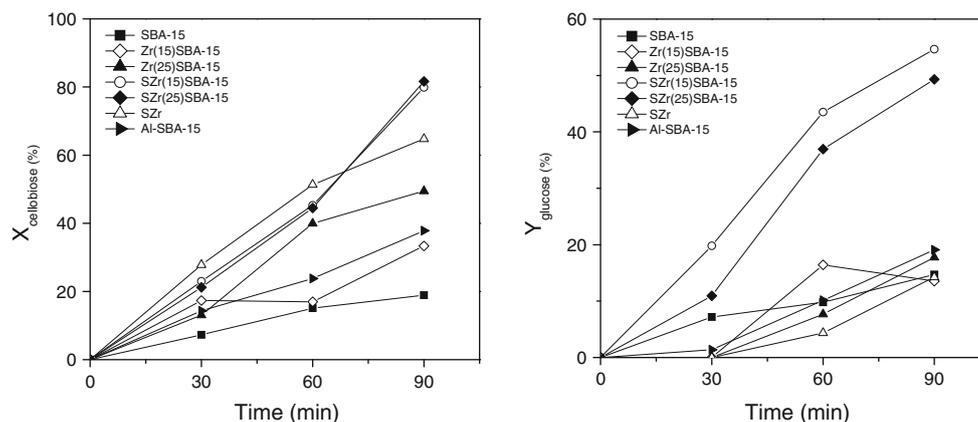


Fig. 8 Cellobiose conversion (*left*) and glucose yield (*right*) as a function of reaction time for a large set of catalysts ($T = 160\text{ }^{\circ}\text{C}$; $p_{\text{N}_2} = 30\text{ bar}$; autoclave; 0.5 wt% cellobiose and 0.1 wt% catalyst in water)

4 Conclusions

Strong Brønsted acidity of sulfated zirconia-SBA-15 catalysts was demonstrated by FTIR spectroscopy of surface hydroxyls upon CO adsorption and TPD of IPAm decomposition. The strong acidity of these materials results from the sulfation of zirconia patches of varying dispersion included in or at the surface of SBA-15. The acidity before sulfation stems from Lewis acidic Zr^{4+} sites. The higher intrinsic Brønsted acidity of a sulfated zirconia modified SBA-15 is close to that of conventional sulfated zirconia. IR spectroscopy suggests that the Brønsted acidity derives from interactions between sulfate groups attached to zirconia and silanol groups. An optimum in the acidity with respect to Zr content is observed. Sulfated zirconia dispersed throughout SBA-15 is an active catalyst for the scission of the 1,4- β glycosidic bonds in cellobiose, which is a model reaction for the critical step in the depolymerization of cellulose into valuable chemicals. The present study suggests that the isolated Brønsted acid sites catalyze cellobiose hydrolysis resulting in high glucose yields.

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