A fully coupled fluid-particle flow solver using quadrature-based moment method with high-order realizable schemes on unstructured grids

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Keywords
kinetic theory of granular flow, QMOM, multiphase flow, unstructured grid, high-order realizable

Disciplines
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Comments

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A fully coupled fluid-particle flow solver using quadrature-based moment method with high-order realizable schemes on unstructured grids

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Abstract

Kinetic Equations containing terms for spatial transport, gravity, fluid drag and particle-particle collisions can be used to model dilute gas-particle flows. However, the enormity of independent variables makes direct numerical simulation of these equations almost impossible for practical problems. A viable alternative is to reformulate the problem in terms of moments of the velocity distribution function. A quadrature method of moments (QMOM) was derived by Desjardins et al. [1] for approximating solutions to the kinetic equation for arbitrary Knudsen number. Fox [2, 13] derived a third-order QMOM for dilute particle flows, including the effect of the fluid drag on the particles. Passalacqua et al. [4] and Garg et al. [3] coupled an incompressible finite-volume solver for the fluid-phase and a third order QMOM solver for particle-phase on Cartesian grids. In the current work a compressible finite-volume fluid solver is coupled with a particle-phase solver based on third-order QMOM on unstructured grids. The fluid and particle-phase are fully coupled by accounting for the volume displacement effects induced by the presence of the particles and the momentum exchange between the phases. The success of QMOM is based on the moment inversion algorithm that allows quadrature weights and abscissas to be computed from the moments of the distribution function. The moment-inversion algorithm does not work if the moments are non-realizable, which might lead to negative weights. Desjardins et al. [1] showed that realizability is guaranteed only with the 1st-order finite-volume scheme that has excessive numerical diffusion. The authors [5, 6] have derived high-order finite-volume schemes that guarantee realizability for QMOM. These high-order realizable schemes are used in this work for the particle-phase solver. Results are presented for a dilute gas-particle flow in a lid-driven cavity with both Stokes and Knudsen numbers equal to 1. For this choice of Knudsen and Stokes numbers, particle trajectory crossing occurs which is captured by QMOM particle-phase solver.

Introduction

Gas-particle flows are relevant in many engineering applications. A detailed understanding of such flows is essential to the improvement of these applications. Currently, there exist several different ways for numerical simulation of gas-particle flows. All of them use the same fluid solver. They differ in the way in which particle phase is treated:

1. Direct solver that discretizes velocity phase space of particle number density function [7, 8].
2. Lagrangian solver that tracks all the particles individually [9].
3. Hydrodynamic models with kinetic theory moment closures [10].
4. Quadrature Method Of Moment (QMOM) solver that solves for moments of particle number density function with quadrature-based closures [1, 2, 4, 11].

A direct solution of the kinetic equation is prohibitively expensive due to the high dimensionality of the space of independent variables, while Lagrangian solvers are computationally very expensive for many engineering and industrial applications, since the number of particles to be tracked is very large. Hydrodynamic models are developed assuming that the Knudsen num-
ber of the flow is nearly zero, which is equivalent to assuming a Maxwellian (or nearly Maxwellian) equilibrium velocity distribution. This, however, is not correct in relatively dilute gas-particle flows, where the Knudsen number is high, the collision frequency is small and phenomena like particle trajectory crossing can happen. In particular, Desjardins et al. [1] showed that the assumption that a gas-particle flow can be described by accounting for only the mean momentum of the particle phase leads to incorrect prediction of all the velocity moments, including the particle number density, showing the need of using a multi-velocity method, in order to correctly capture the physics of the flow.

Q MOM for gas particle flow [2, 12, 13] is based on the idea of tracking a set of velocity moments of arbitrarily high order, providing closures to the source terms and the moment spatial fluxes in the moment transport equations by means of a quadrature approximation of the number density function. Fox [2, 13] derived a third order Q MOM for dilute particle flows, including the effect of the fluid drag on the particles. Passalacqua et al. [4] and Garg et al. [3] coupled a third order Q MOM solver with an incompressible finite-volume solver for the fluid-phase on Cartesian grids. In the current work, a compressible finite-volume fluid-phase solver is coupled with a particle phase solver based on third-order Q MOM on unstructured grids. The fluid and particle phases are fully coupled by accounting for the volume fraction, density, velocity components and pressure respectively. The total energy \( E^f \) can be written as:

\[
E^f = \frac{p^f}{(\gamma - 1) \rho^f} + \frac{1}{2} \rho^f U_{ij} U_{ij},
\]

where \( \gamma \) is the ratio of specific heats. In (4), the components of the viscous stress tensor \( \sigma_{\alpha ij} \) are given by

\[
\sigma_{\alpha ij} = \mu^f \left( \frac{\partial U_{\alpha i}}{\partial x_j} + \frac{\partial U_{\alpha j}}{\partial x_i} \right) - \frac{2}{3} \mu^f \frac{\partial U_{\alpha k}}{\partial x_k} \delta_{ij},
\]

where \( \mu^f \) is the fluid dynamic viscosity and \( \delta_{ij} \) denotes Kronecker delta. The body force due to gravity is accounted for by \( \alpha_Tr \). For the current work, gravity is not considered. The other two source terms, \( M_{\rho p} \) and \( Q_{\rho p} \) account for momentum and energy exchange between the fluid and particle phases. Details about these two source terms will be discussed in a later section.

Fluid-phase governing equations

The fluid-phase is described by Navier-Stokes equations modified for multi-fluid models. The fluid-phase continuity, momentum and energy equations are given as:

\[
\frac{\partial W^f_i}{\partial t} + \frac{\partial H^f_{ij}(W^f_i)}{\partial x_j} = \frac{\partial H^f_{ij}(W^f_i)}{\partial x_j} + S^f_i.
\]

In (1), \( W^f_i, H^f_{ij}(W^f_i), H^f_{ij}(W^f_i) \) and \( S^f_i \) denote the set of conserved variables, inviscid fluxes, viscous fluxes and source terms respectively. These terms are given by

\[
W^f_i = \begin{bmatrix}
\alpha f p \\
\alpha f \rho^f U_{\alpha i} \\
\alpha f \rho^f E^f_i
\end{bmatrix},
\]

\[
H^f_{ij}(W^f_i) = \begin{bmatrix}
\alpha f \rho^f U_{ij} \\
\alpha f \left( \rho^f U_{\alpha i} U_{\alpha j} + p^f \right) \\
\alpha f \left( \rho^f E^f_i + p^f U_{\alpha j} \right)
\end{bmatrix},
\]

\[
H^f_{ij}(W^f_i) = \begin{bmatrix}
0 \\
\sigma_{\alpha ij} U_{\alpha i} \\
\sigma_{\alpha ij} U_{\alpha i}
\end{bmatrix},
\]

\[
S^f_i = \begin{bmatrix}
0 \\
M_{\rho p} + \alpha_f g^f_i \\
Q_{\rho p}
\end{bmatrix}.
\]
Particle-phase governing equations

Kinetic equation. Dilute gas-particle flows can be modeled by a kinetic equation [14, 15, 16] of the form:

\[ \partial_t f + \mathbf{v} \cdot \partial_x f + \partial_v \cdot (f \mathbf{F}) = C, \]  

where \( f(\mathbf{v}, \mathbf{x}, t) \) is the velocity based number density function, \( \mathbf{v} \) is the particle velocity, \( \mathbf{F} \) is the force acting on individual particle, and \( C \) is the collision term representing the rate of change in the number density function due to collisions. The collision term can be described using Bhatnagar-Gross-Krook (BGK) collision operator [17]:

\[ C = \frac{1}{\tau_c} (f_{eq} - f), \]  

where \( \tau_c \) is the characteristic collision time, and \( f_{eq} \) is the Maxwellian equilibrium number density function given by:

\[ f_{eq}(\mathbf{v}) = \frac{M^0}{\sqrt{(2\pi\sigma_{eq})^3}} \exp \left( -\frac{\mathbf{v} - \mathbf{U}_p}{2\sigma_{eq}} \right), \]  

in which \( \mathbf{U}_p \) is the mean particle velocity, \( \sigma_{eq} \) is the equilibrium variance and \( M^0 = \int f d\mathbf{v} \) is the particle number density. In fluid-particle flows, the force term is given by the sum of the gravitational contribution and the drag term exerted from the fluid on the particles.

Moment transport equations. In the quadrature-based moment method of Fox, a set of moments of number density function \( f \) are transported and their evolution in space and time is tracked. Each element of the moment set is defined through integrals of the velocity distribution function. For the first few moments the defining integrals are:

\[
\begin{align*}
M^0 & = \int f d\mathbf{v}, \\
M^1_{ij} & = \int v_i v_j f d\mathbf{v}, \\
M^2_{ij} & = \int v_i v_j v_k f d\mathbf{v}, \\
M^3_{ijk} & = \int v_i v_j v_k v_l f d\mathbf{v}.
\end{align*}
\]

In these equations, the superscript of \( M \) represents the order of corresponding moment. The particle-phase volume fraction \( \alpha_p \) and mean particle velocity \( \mathbf{U}_p \) are related to these moments by:

\[ \alpha_p = V_p M^0 \]  

and

\[ \rho_p \mathbf{U}_p = m_p M^1_{i}. \]  

where \( m_p = \rho_p V_p \) is the mass of a particle with density \( \rho_p \) and volume \( V_p \). For 2D cases, \( V_p = \pi d_p^2 / 4 \) and for 3D cases, \( V_p = \pi d_p^3 / 6 \). Likewise, the particle temperature is defined in terms of the trace of the particle velocity covariance matrix, which is found from \( M^2_{ij} \) and lower-order moments. By definition, \( \alpha_p + \alpha_f = 1 \) and this relation must be accounted for when solving a fully coupled system for the fluid and particle phases.

Moment transport equations are obtained by applying the definition of moments to (8). The transport equations for moments in (11) can be written as:

\[ \frac{\partial W_p}{\partial t} + \frac{\partial H_{pl}(W_p)}{\partial x_l} = D_p + G_p + C_p. \]  

In (14), \( W_p \) and \( H_{pl}(W_p) \) are the conserved moments and spatial fluxes respectively and are given as:

\[ W_p = \begin{bmatrix} M^0 \\ M^1_{i} \\ M^2_{ij} \\ M^3_{ijk} \end{bmatrix}, \]  

\[ H_{pl}(W_p) = \begin{bmatrix} M^1_{i} \\ M^2_{ij} \\ M^3_{ijl} \end{bmatrix}. \]  

The source terms on right hand side of (14), \( D_p, G_p \) and \( C_p \) respectively denote drag, gravity and collision terms and can be written as:

\[ D_p = \begin{bmatrix} 0 \\ D^1_{i} \\ D_{ij} \\ D_{ijk} \end{bmatrix}, \]  

\[ G_p = \begin{bmatrix} 0 \\ 0 \\ g_i M^0 + g_j M^1_{ij} \\ g_i M^2_{ij} + g_j M^2_{ij} + g_k M^3_{ijk} \end{bmatrix}, \]  

\[ C_p = \begin{bmatrix} 0 \\ 0 \\ C^0_{ij} \\ C_{ijk} \end{bmatrix}. \]  

Gravity is not considered in the current work. Hence, \( G_p = 0 \). The details of drag and collision terms will be discussed later.

According to the third order QMOM derived by Fox [2, 13], following set of moments are transported in 2D and 3D respectively:

\[
W_p^{2D} = [M^0, M^1_{i}, M^2_{ij}, M^3_{ijl}, M^3_{i}]
\]

\[
W_p^{3D} = [M^0, M^1_{i}, M^2_{ij}, M^3_{ijl}, M^3_{ijk}, M^3_{i}]
\]
The method based on (22) is called \( \beta \)-node quadrature method. The moments can be computed as a function of quadrature weights and abscissas by using the above definition of \( f \) in (7):

\[
\begin{align*}
M^0 &= \sum_{\alpha=1}^{\beta} n_\alpha, \\
M^1 &= \sum_{\alpha=1}^{\beta} n_\alpha U_{\alpha i}, \\
M^2 &= \sum_{\alpha=1}^{\beta} n_\alpha U_{\alpha i} U_{\alpha j}, \\
M^3 &= \sum_{\alpha=1}^{\beta} n_\alpha U_{\alpha i} U_{\alpha j} U_{\alpha k},
\end{align*}
\]

(23)

For simplicity, hereinafter we will assume that all of the moments have been multiplied by \( V_p \), so that the zero order moment corresponds to the particle-phase volume fraction \( M^0 = \alpha_p \). This simplification helps in handling of coupling terms.

**Quadrature-based closures.** Using the BGK model [17], the collision terms in (19) can be closed. Details of closure of collision terms can be found in [4]. However, the set of transport equations in (14) is still unclosed because of the spatial flux and drag terms. Each equation contains the spatial fluxes of the moments of order immediately higher. In quadrature-based moment methods, quadrature formulas are used to provide closures to these terms in the moment transport equations, by introducing a set of weights and abscissas. The number density function \( f \) is written in terms of the quadrature weights \( (n_\alpha) \) and abscissas \( (U_{\alpha}) \) using Dirac delta representation:

\[
f(v) = \sum_{\alpha=1}^{\beta} n_\alpha \delta(v - U_{\alpha}).
\]

(22)

The next few sections discuss the details of the fluid and particle phase solvers and the coupling between them. Although, for the numerical simulations a two-stage Runge-Kutta scheme is used, for simplicity, all the discussion on solver details and coupling algorithm will be based on a single-stage time-integration.

**Fluid-phase solver**

Let \( I \) and \( \partial I \) denote any cell in the domain and its boundary respectively. Also let \( e \in \partial I \) be a face of cell \( I, A_e \) be its area and \( I_{eb} \) be the neighbouring cell corresponding to this face. The finite-volume scheme using single-stage explicit time-integration for (1) can be written as:

\[
\begin{align*}
W^{n+1}_I &= W^n_I - \frac{\Delta t}{\text{vol}_I} \sum_{e \in \partial I} \left\{ G_e \left( W^n_{le}, W^n_{le,nb} \right) A_e \right\} \\
&\quad + \frac{\Delta t}{\text{vol}_I} \sum_{e \in \partial I} \left\{ G^n_e \left( W^n_{le}, W^n_{le,nb} \right) A_e \right\} \\
&\quad - \Delta t S_e,
\end{align*}
\]

(30)
where $W^n_{e_l}$ and $W^{n+1}_{e_l}$ are the cell averaged values while $W^n_{e_l|e_{l,nb}}$ and $W^n_{e_l|e_{l,nb},e_{l}}$ are the values reconstructed on different sides of the face $e$. Also, $vol_I$ denotes the volume of cell $I$. In (30), $G_I$ and $G^n_I$ denote numerical inviscid and viscous fluxes respectively. Roe flux [19] is used to calculate $G_I$. For calculation of viscous flux, gradient of velocity field is required which is obtained using $BGK$ model as:

$$\frac{n_\alpha}{n_{e}}U_{\alpha} = \frac{n_\alpha}{n_{e}}U_{\alpha} I_{\epsilon} + \eta (U^n_{\alpha} - U_{\alpha} I_{\epsilon})$$

Collision terms. Collisions only affect the second and third order moments. These moments are updated using $BGK$ model as:

$$W^n_{pl} = \Delta t_{pl} + (W^n_{pl} - \Delta t_{pl})\exp(-\Delta t/\tau_c),$$

where $\tau_c$ is the collision time and $\Delta t_{pl}$ denotes the set of equilibrium moments. Details about the calculation of $\tau_c$ and $\Delta t_{pl}$ can be found in [4].

Drag terms. Drag terms do not affect the weights because they do not change the number of particles. The weights obtained after accounting for collisions in (33) are updated using:

$$U^{n+1}_{\alpha I_{\epsilon}} = U^{**}_{\alpha I_{\epsilon}} + \Delta t_{\alpha I_{\epsilon}} F^{**}_{\alpha I_{\epsilon}}$$
3. Pass $\Delta t_f$, $\rho_f$, $\mu_f$, $U_f$ from fluid-phase solver to particle-phase solver.

4. For the particle-phase solver calculate $\Delta t_p$. Details of calculation of $\Delta t_p$ can be found in [6].

5. Calculate global time step, $\Delta t = \min(\Delta t_f, \Delta t_p)$.

6. Advance particle-phase solver by $\Delta t$.
   a) Advance moments by $\Delta t$ due to spatial flux terms using a finite-volume approach.
   b) Advance moments by $\Delta t$ due to collision terms.
   c) Advance weights by $\Delta t$ due to drag force terms and compute the coupling source terms $M_{fp}$ and $Q_{fp}$ for fluid-phase solver.

7. Pass $\Delta t$, $M_{fp}$, $Q_{fp}$ and $\alpha_f (= 1 - \alpha_p)$ from particle-phase solver to fluid-phase solver.

8. Advance fluid-phase solver by $\Delta t$.

9. Repeat steps 2 through 8 at each timestep.

**Numerical Results**

Numerical results are presented for a dilute gas-particle flow in a lid-driven cavity. The lid has a length $L$ and moves with a constant velocity $U_{lid}$, as schematized in Figure 1. The cavity is filled with the gas phase and with initially uniformly distributed particles. Both the phases have zero initial velocity as initial condition. The evolution of the flow fields are tracked for a time sufficient to the lid to go through twenty lid lengths. The parameters that characterize the system are the Knudsen number ($Kn$), the Reynolds number ($Re$), the Stokes number (St) and the mass loading ($\lambda$). The Knudsen number is defined as:

$$Kn = \frac{d_p}{6\alpha_p L\sqrt{2}}.$$  \hspace{1cm} (35)

The Reynolds number is defined on the base of the lid length and the lid velocity as:

$$Re = \frac{\rho_f |U_{lid}|L}{\mu_f}.$$  \hspace{1cm} (36)

The mass loading is given by the ratio

$$\lambda = \frac{\alpha_g \rho_g}{\alpha_f \rho_f},$$  \hspace{1cm} (37)

while Stokes number is defined as:

$$St = \frac{1}{18} \frac{\rho_p}{\rho_f} \left( \frac{d_p}{L} \right)^2 Re.$$  \hspace{1cm} (38)

Results are presented for the case with $Kn = 1$, $St = 1$, $Re = 100$, $\lambda = 2.5$. This case is of particular interest as it involves particle trajectory crossing which cannot be captured by two-fluid models [3]. Particles are driven by the fluid velocity field. At the top-right corner particles hit the wall and are reflected back. Because of particles with opposing velocities, trajectory crossing occurs near the top-right corner. Figure 2 shows the grid with rectangular cells near the boundary and triangular cells in the core region. Total number of cells is 6904. A two stage Runge Kutta scheme is used for time-integration. Figure 3 and Figure 4 show particle volume-fraction fields at the final time. Figure 3 shows results when 1$^{st}$-order finite-volume scheme is used for both fluid and particle phase solvers while Figure 4 shows results when 2$^{nd}$-order finite-volume scheme is used for fluid-phase solver and quasi-2$^{nd}$-order [5, 6] finite-volume scheme is used for particle-phase solver. Both Figure 3 and Figure 4, show the trajectory crossing near the top-right corner. The results are in agreement with the ones presented in [3]. Second-order finite-volume solver for the fluid phase gives better resolution of the fluid velocity field. As the particles are driven by the fluid velocity field, a second-order finite-volume solver for fluid-phase leads to better prediction of particle volume-fraction. The use of quasi-2$^{nd}$-order finite-volume scheme for particle-phase further improves the solution.

**Conclusions**

In the current work, a compressible finite-volume fluid solver is coupled with a particle-phase solver based on third-order QMOM on unstructured grids. The fluid and particle-phase are fully coupled by accounting for the volume displacement effects induced by the presence of the particles and the momentum exchange between the phases. High-order realizable finite volume schemes are
used for particle-phase QMOM solver. Numerical results are presented for a dilute gas-particle flow in a lid-driven cavity. Complex features like particle-trajectory crossing are captured easily. The coupling can be extended to practical problems as it is relatively inexpensive compared to Lagrangian and direct kinetic solvers.

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References


